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The Efficiency of Strontium-90 Desorption Using Iron (III) Solutions in the Decontamination Process of Radioactive Soils

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ABSTRACT

The paper presents the investigation on the estimated efficiency of iron (III) chloride solutions in the decontamination process of radioactive soils with ⁹⁰Sr, according to kinetic and thermodynamic characteristics of the desorption process. The specific ⁹⁰Sr radioactivity of soil samples was $(3.9\pm0.3)\cdot10^4$ Bq·g. The adsorption isotherms of Sr²⁺ and Fe³⁺ are described with the Langmuir equation. The values of Gibbs energy G⁰₂₉₈ = -4.65 kJ·mol⁻¹ and equilibrium ion exchange constant K_{eq} = 6.5 confirm the hypothesis of strontium removal from soils with iron (III) cations. The effectiveness of the method is substantiated by experimental and calculated results of this study samples of radioactive soils are deactivated in 90% after 9.5 hours, whereas the kinetic constant is 6.77·10 s⁻¹. The suggested method of soil cleanup with 0.2 M Fe³⁺ solutions is optimal and complies with the environmental requirements.

Keywords: decontamination of radionuclides, thermodynamic and kinetics investigations, desorption of strontium-90, iron (III) chloride.

INTRODUCTION

Radioactive isotopes of heavy metals are considered to be particularly dangerous matter which is produced in the course of anthropogenic activities, industrial accidents and nuclear tests. Strontium-90 isotope is mainly fixed on the surface of clay minerals [Bobovnikova 1990]. Radionuclides undergo physicochemical reactions on the border between solid and liquid phases in soils, where strontium is found in different forms. There are cations of radionuclides in the soil solution and cations which are fixed in solid (non-exchangeable). Fixation of exchangeable form and remobilization of fixed radionuclides are caused by cations diffusion in solid particles [Bulgakov 1998, Bondarenko and Kononenko 2001]. The majority of water-soluble 90Sr (76%) occurs in cation forms [Martyushov et al. 1995].

The authors Ningping and Mason [2001] propose strontium-free ground water for Sr(II) removal from silica colloids and Ca-montmoril-

lonites. The desorption from montmorillonites is a time-consuming and ineffective process – the amount of recovered strontium is 16.5% after 90 days. Desorption in the study [Martyushov et al. 1995] was executed with different concentrations of HCl and HNO₃. The most effective outcome was achieved with 0.1 M solutions – 83% and 82% for HCl and HNO₃, respectively. However, strong acids are too expensive and they form acidic soils which are not applicable.

The review of the literature on the ⁹⁰Sr desorption process indicates that there is a need to detect an eluent for radioactive soils recultivation which is safe and provides effective desorption parameters.

It was proposed that ion exchange of strontium with high complex formation properties will promote the extraction of radionuclides from soils. Cations of Fe^{3+} are characterized by a high charge and a small radius. Due to the high ionic potential, which is equal to z/r, Fe^{3+} displaces other cations from mineral surface, including ¹³⁷Cs and ⁹⁰Sr. Therefore, it was suggested to apply iron (III) chloride solutions with ammonium chloride (for pH stabilization) for soils decontamination.

The aim of this investigation was to estimate the efficiency of iron (III) chloride solutions in the decontamination process of radioactive soils with ⁹⁰Sr according to kinetic and thermodynamic characteristics of the desorption process.

MATERIALS AND METODS

The process of sorption was performed on samples using water solutions with the specific radioactivity of 10^{-5} Ci·dm⁻³. The process was carried out with the limited value method. The sample weight was brought into contact with the ⁹⁰Sr solution, interblended roundly with a churn over two weeks in order to obtain a stable solution. The solid phase was separated from the liquid phase and washed with distilled water. The specific ⁹⁰Sr radioactivity of soil samples was $(3.9\pm0.3)\cdot10^4$ Bq·g⁻¹.

The ⁹⁰Sr desorption was applied dynamically. It was chosen to apply 0.02 mol·dm⁻³ iron (III) chloride as an eluent solution. The process was held in a 5 cm height glass column with the cross-sectional area of 0.7 cm² and the interstitial volume of 3 cm². The underside of the column was filled with glass fiber and a Sr-adsorbed soil sample of 2 g weight above it. The desorption agent was carried through the solid structure with the 9·10⁻⁴ m·s⁻¹ rapidity. After 3 cm³ of the eluent passed the column, 5 and 10 ml portions were collected and their ⁹⁰Sr radioactivity was analyzed. If there are both ⁹⁰Sr and ¹³⁷Cs radionuclides in soils, it is necessary to supplement ammonium chloride as a cesium carrier.

Real contaminated soil patterns were collected in the area which is 15 away from the 4th plant unit of the Chernobyl Electric Power Station.

RESULTS AND DISCUSSION

The adsorption isotherms of Sr2+ and Fe3+ are described with the Langmuir equation and shown in Figure 1, where $\nabla \infty$ is equilibrium concentration of the cations, g – the activity factor and DS/L is the distribution constant between the solid and liquid phases.

Figure 2 shows the linear dependence between the inverse of sorption and concentration. The equations are $\frac{1}{\Gamma} = 0.1075 \frac{1}{C} + 26.588$ and $\frac{1}{\Gamma} = 0.0512 \frac{1}{C} + 42.18$ for strontium and iron (III), respectively. This result is in accordance with the study [Chirkst et al. 1994, Chirkst et al. 2003], where effectiveness of the Langmuir equation is described for cesium cations sorption on a variety of minerals.

The absolute term of the Langmuir equation is equal to the inverse of the limit value of sorption, which is 0.034 mol·kg⁻¹ for Sr^{2+} and 0.024 mol·kg⁻¹ for Fe³⁺. Slope ratios were used to determine the adsorption thermodynamic equilibrium ratios of strontium and iron on clay minerals which are 294 and 731, respectively.

The distribution coefficient of strontium between the solid and liquid phases depends on strontium (2+) concentration in equilibrium solution and coverage ratio of the adsorbent:



Figure 1. The sorption isotherms of strontium (a) and iron (3+) cations (b) on clay minerals

| Sr ²⁺ | | | Fe ³⁺ | | |
|--|------------------------|------------------|--|------------------------|------------------|
| C _∞ ·10 ⁴ , mol·dm ⁻³ | $\gamma_{\rm Sr}^{2+}$ | D _{s/L} | C _∞ ·10 ⁴ , mol·dm ⁻³ | $\gamma_{\rm Fe}^{3+}$ | D _{s/L} |
| 0.42 | 0.92 | 15.0 | 1.28 | 0.73 | 2.8 |
| 1.05 | 0.89 | 10.2 | 1.84 | 0.58 | 27.5 |
| 2.08 | 0.85 | 10.8 | 2.38 | 0.54 | 31.3 |
| 3.33 | 0.83 | 9.7 | 2.53 | 0.53 | 31.1 |
| 4.36 | 0.80 | 10.4 | 5.24 | 0.41 | 43.6 |
| 5.55 | 0.80 | 10.0 | 16.9 | 0.30 | 22.5 |
| 11.3 | 0.72 | 10.7 | 27.9 | 0.23 | 23.5 |
| 18.9 | 0.67 | 9.8 | 35.5 | 0.20 | 27.4 |
| 50 | 0.56 | 7.2 | 46.1 | 0.18 | 18.5 |
| 65 | 0.52 | 7.4 | | | |
| 73 | 0.51 | 7.3 | | | |
| 172 | 0.44 | 3.7 | | | |
| 371 | 0.34 | 0.23 | | | |

Table 1. Characteristics of Sr²⁺ and Fe³⁺ distribution between the solution and clay samples



Figure 2. Linear form of the sorption isotherm for strontium (2+) (a) and iron (b) on clay minerals

$$D_{\mathrm{T/m}} = \frac{\Gamma_{\infty} \mathrm{K}}{\gamma_{\mathrm{Sr}^{2+}} (1 + \mathrm{Kc}_{\infty})} \tag{1}$$

However, limit dilution brings about the value of $D_{S/L} = \Gamma_{\infty} K = 10.0$ which is the same as the experimental result (Table 1). For the $Sr^{2+}_{aq} \Leftrightarrow Sr^{2+}_{aac}$ equilibrium, which characterizes the sorption ability of a strontium cation, the value of Gibbs energy is $\Delta G^{0_{298}} = -RT \ln D_{S/L} = -5.7 \text{ kJ/mol}$. This value illustrates rising of the sorption ability in response to hydroxonium cations transition with strontium cations due to increase of the charge.

According to the study [Thermodynamic constants... 1981], under the condition of $\Delta_f G^{0_{298}}(\mathrm{Sr}^{2+_{aq}}) = -563.9 \, kJ/\mathrm{mol}$, the value of Gibbs energy for adsorbed cation formation is $\Delta_f G^{0_{298}} = -569.6 \, kJ/\mathrm{mol}$. The following equations are defined with the distribution coefficient of Fe³⁺ and the Langmuir constant:

$$\operatorname{Fe}^{3+}_{aq} \Leftrightarrow \operatorname{Fe}^{3+}_{ads}$$
 (2)

$$Fe(OH)^{2+}_{aq} \Leftrightarrow Fe(OH)^{2+}_{ads}$$
 (3)

$$\operatorname{Fe}(\operatorname{OH})_{2^{+}aq} \Leftrightarrow \operatorname{Fe}(\operatorname{OH})_{2^{+}ads}$$
(4)

The main forms of iron (3+) in solutions with the value of pH 3.1 are taken into account with corresponding thermodynamic characteristics. The sorption of iron (III) polymeric forms is neglected. The summary of the equations (5)-(7) describes the adsorption process of iron (III) with m, n and p coefficients:

$$\frac{n}{m} = \frac{[\text{Fe}(\text{OH})^{2+}]}{[\text{Fe}^{3+}]} = \frac{K_{h,1}}{[H^+]}$$
(5)

$$\frac{p}{n} = \frac{[\text{Fe(OH)}_{2^+}]}{[\text{Fe(OH)}^{2^+}]} = \frac{K_{h,2}}{[H^+]}$$
(6)

$$m+n+p=1\tag{7}$$

Hydrolysis constants of iron (3+) are $K_{h,1} = 6.74 \cdot 10^{-3}$ and [9]. Hydroxonium cations concentration is found due to pH = 3.1. Consequently, m = 0.024. n = 0.20 and p = 0.776. The summary equation of the iron (III) adsorption process is:

$$0.024 \text{ Fe}^{3+}_{aq} + 0.2 \text{ Fe}(\text{OH})^{2+}_{aq} + + 0.776 \text{ Fe}(\text{OH})_{2+}^{2}_{aq} \Leftrightarrow \Leftrightarrow 0.024 \cdot \text{Fe}^{3+}_{ads} + 0.2 \text{Fe}(\text{OH})^{2+}_{ads} + + 0.776 \text{ Fe}(\text{OH})_{2+}^{2}_{ads}$$
(8)

Using the summary distribution coefficient, it is possible to determine the Gibbs energy for the reaction (8): $\Delta_{(8)}G^0_{298} = \Delta \text{ RTln } D_{S/L} = -8.2\pm0.3 \text{ kJ}\cdot\text{mol}^{-1}$.

In order to calculate the equilibrium constants for (2)-(4), it is necessary to make a series of operations.

$$\Delta_{(8)}G^{0}{}_{298} = m \Delta_{(2)}G^{0}{}_{298} + + n \Delta_{(3)}G^{0}{}_{298} + p \Delta_{(4)}G^{0}{}_{298}.$$
 (9)

Then:
$$D = D_1^m \cdot D_2^n \cdot D_3^p$$
, (10)

where: *D* is the experimental summarized distribution coefficient of iron (III), D_n – partial distribution coefficients of different iron forms for the equations (2)-(4), and their values are:

$$D_1 = \frac{[Fe^{3+_{ads}}]}{[Fe^{3+_{aq}}]}$$
(11)

$$D_2 = \frac{[\text{Fe}(\text{OH})^{2+_{\text{ads}}}]}{[\text{Fe}(\text{OH})^{2+_{\text{aq}}}]}$$
(12)

$$D_3 = \frac{\left[\operatorname{Fe}(\operatorname{OH})_{2_{\operatorname{ads}}^+}\right]}{\left[\operatorname{Fe}(\operatorname{OH})_{2_{\operatorname{aq}}^+}\right]} \tag{13}$$

$$D = \frac{[\text{Fe}(\text{OH})^{2+}_{\text{ads}}] + [\text{Fe}(\text{OH})_{2^+_{\text{ads}}}]}{C}$$
(14)

The sorption of Fe^{3+} ions is neglected in (14) due to their small concentration. Calculating (11)-(14), the values of D₂ and D₃ are:

$$D_{3} = \frac{D \cdot C - [Fe(OH)^{2+_{ads}}]}{[Fe(OH)_{2^{+}_{aq}}]}$$

$$= \frac{D \cdot C - K_{2} \cdot [Fe(OH)^{2+_{aq}}]}{[Fe(OH)_{2^{+}_{aq}}]}$$
(15)

The values D = 27, [Fe(OH)^{2+aq}] = 0.776C, [Fe(OH)_{2aq}] = 0.2*C* are substituted into the equation (15). Calculating together the equations (11) and (14), where the exchange coupling constant is approximately 1 (and D₁ \approx D₂^{1.5}, D₂ \approx D₃² μ D₁ \approx D₂·D₃), the distribution constants are D₁=1200, D₂=60 and D₃=20. Then $\Delta_{(2)}G^{0}_{298}$ = -17.6 kJ· mol⁻¹, $\Delta_{(3)}G^{0}_{298}$ = - 10.2 kJ· mol⁻¹ and $\Delta_{(4)}G^{0}_{298}$ = - 7.4 kJ· mol⁻¹. Table 2 shows the calculated Gibbs energy of adsorbed iron (3+) cations formation and sorption equilibrium.

Furthermore, there are three exchange reactions:

$$13Fe^{3+aq} + 12Sr^{2+ads} \Leftrightarrow$$

$$\Leftrightarrow 13Fe^{3+ads} + 12Sr^{2+aq}$$

$$\Delta_{(16)}G^{0}_{298} = -3.02 \text{ kJ} \cdot \text{equiv}^{-1};$$

$$K_{(16)} = 3.4.$$
(16)

$$12Fe(OH)^{2+aq} + 12Sr^{2+ads} \Leftrightarrow \Leftrightarrow 12Fe(OH)^{2+ads} + 12Sr^{2+aq} \Delta_{(17)}G^{0}_{298} = -2.25 \text{ kJ} \cdot \text{equiv}^{-1};$$
(17)
 $K_{(17)} = 2.5.$

$$Fe(OH)_{2_{aq}^{+}} + 12Sr^{2+_{ads}} \Leftrightarrow$$

$$\Leftrightarrow Fe(OH)_{2_{ads}^{+}} + 12Sr^{2+_{aq}}$$

$$\Delta_{(18)}G^{0}_{298} = -4.55 \text{ kJ} \cdot \text{equiv}^{-1};$$

$$K_{(18)} = 6.3.$$
(18)

The Gibbs energy for the summary ion exchange reaction with strontium is:

$$\Delta_{\Sigma} G^{0}_{298} = 0.072 \Delta_{(16)} G^{0}_{298} + 0.4 \Delta_{(17)} G^{0}_{298} + 0.776 \Delta_{(18)} G^{0}_{298} = -4.65 \text{ kJ} \cdot \text{mol}^{-1}.$$

Consequently, the total ion exchange equilibrium constant is 6.5. It means that strontium cations will expel from clay minerals after a leaching operation with iron (III) solutions.

Iron (III) chloride solutions were used for strontium desorption from clay minerals. According to the experimental data (Figure 3), the kinetic coefficient of ⁹⁰Sr sorption on modelling samples is 2.9·10⁻⁴ s⁻¹ through the Wigner-Polanyi equation. The initial specific ⁹⁰Sr radioac-

| Reaction | $\Delta_{f}G^{0}_{298}(Kat^{z+}_{q}),$ kJ·mol ⁻¹ [147] | $\Delta_f G^0_{298}(Kat^{z+}_{ads})$ kJ·mol ⁻¹ | $\Delta_{_f}G^0{}_{_{298}}$, kJ \cdot mol $^{	extsf{-1}}$ | K _{eq} |
|--|--|--|--|-----------------|
| $Fe^{3+}_{aq} \leftrightarrow Fe^{3+}_{ads}$ | -4.52 | -22.1 | -17.6 | 1200 |
| $Fe(OH)^{2+}_{aq} \leftrightarrow Fe(OH)^{2+}_{ads}$ | -229.37 | -239.6 | -10.2 | 60 |
| $Fe(OH)_{2 \text{ aq}}^{+} \leftrightarrow Fe(OH)_{2 \text{ ads}}^{+}$ | -452.29 | -459.7 | -7.4 | 20 |
| $\mathrm{Sr}^{2+}_{\mathrm{aq}} \leftrightarrow \mathrm{Sr}^{2+}_{\mathrm{ads}}$ | -563.9 | -569.6 | -5.7 | 10 |

Table 2. Thermodynamic characteristics of iron and strontium cations adsorption on clay minerals



Figure 3. Desorption kinetics of ⁹⁰Sr from modelling samples

tivity of soils is $(3.9\pm0.3)\cdot10^4$ Bq·g⁻¹. As a result, the time required to achieve 90% desorption is approximately 2.2 hours.

After the process of ablution, the value of initial specific 90 Sr radioactivity changed from 7.23 \cdot 10 2 Bq \cdot g⁻¹ to 1.87 \cdot 10 2 Bq \cdot g⁻¹. As a consequence, the extent of desorption is 75±5%. The kinetic constant for natural soil samples is 6.77 \cdot 10 c⁻¹ and the period of 90% desorption is 9.5 hours. Accordingly, the kinetic constant of real samples sorption is 5 times bigger than modelling samples.

CONCLUSIONS

The values of Gibbs energy G_{298}^{0} =-4.65 kJ·mol⁻¹ and equilibrium ion exchange constant $K_{eq} = 6.5$ confirm the hypothesis of strontium removal from soils with iron (III) cations. The effectiveness of this method is substantiated by experimental and calculated results of this study samples of radioactive soils are deactivated in 90% after 9.5 hours, the kinetic constant is 6.77·10 s⁻¹. The suggested method of soil cleanup with 0.2 M Fe³⁺ solutions is optimal and complies with environmental requirements.

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