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# Primary treatment of fishery wastewater using chemical and natural coagulants

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#### **ABSTRACT**

The Peruvian fishing industry is responsible for generating large volumes of effluents, whose treatment is complicated due to their high content of salts, organic matter and total suspended solids (TSS). The coagulation-flocculation method, utilizing chemical agents, has been employed for this purpose due to its efficacy. However, given that its use has negative impacts on health and the environment, the search for sustainable alternatives is a priority. In that sense, the objective of this study was to evaluate the efficacy of natural coagulants (chitosan and *Moringa oleifera* seeds powder) and chemicals (ferric chloride) to reduce total dissolved solids (TDS) in fishery wastewater. To that end, coagulant solutions were prepared, wastewater samples were collected to perform jar tests based on the established operating conditions, and finally, the reduction percentages were calculated. The results showed that natural coagulants are more effective than chemical coagulants to reduce TDS. Specifically, the application of chitosan and *Moringa oleifera* seeds powder generated maximum reductions of  $98 \pm 0.71\%$  and  $86.98 \pm 1.92\%$ , respectively, at a dose of 160 mg/0.5 L, while ferric chloride produced a maximum decrease of  $83.64 \pm 0.14\%$  at a dose of 120 mg/0.5 L. Therefore, those findings support the idea that natural coagulants represent an effective and sustainable way to reduce physicochemical parameters from water.

**Keywords:** chitosan, *Moringa oleifer*a seeds, ferric chloride, coagulation-flocculation, fishery wastewater, total dissolved solids.

### INTRODUCTION

Globally, the fishery sector represents a highly relevant economic activity, because it provides food resources as well as generates employment opportunities for millions of people (González et al., 2025). Those opportunities benefit those who are directly engaged in fishing and who are involved in the entire production chain, including vessel construction, equipment supply and marketing of fishery products on large and small scales (Tursi et al., 2015). According to food and agriculture organization (FAO, 2016), artisanal fishing contributes approximately 40% of the world's catch and provides a livelihood for 90% of the people involved in fishing. In Peru, more than 64% of hydrobiological products for direct human consumption come from artisanal fishing, highlighting its importance as an economic

activity for thousands of families (Ministry of Production [PRODUCE], 2020).

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To ensure proper sanitary conditions during the landing, handling, storage and marketing of hydrobiological resources from artisanal fishing, the National Fund for Fisheries Development (FONDEPES) oversees the implementation of Artisanal Fishing Landing Sites (DPA), which are facilities required to achieve minimum sanitary standards for carrying out each of the stages (PRODUCE, 2020).

The series of post-capture stages requires large quantities of water for cleaning operations (Liu et al., 2022), which in turn generates significant volumes of wastewater. According to Al-Dawery et al. (2023), nearly 30% of the total volume of industrial effluents originates from activities related to fishing and fishery product processing. Wastewater from fishing activities is characterized by the

presence of blood, feces, tissues, salts, oils and fats (Anh et al., 2021; Ayyoub et al., 2022). Those components contribute high concentrations of nutrients such as nitrogen and phosphorus as well as organic matter and other contaminants associated with physicochemical parameters such as turbidity, total suspended solids (TSS) and total dissolved solids (TDS) (Ribeiro and Juarez, 2021). Regarding this last parameter, it is important to mention its great relevance in fishing effluents, since they are characterized by the high content of dissolved organic matter such as blood, mucus and undissolved fats generated during the washing, cutting and gutting of hydrobiological resources (Kusumanti et al., 2021). Moreover, TDS are more difficult to eliminate through conventional treatments for fishing effluents (Pushpalatha et al., 2022).

Based on Singh and Kumar (2020), effluents pose an environmental threat if they are not treated but are discharged directly into surface water bodies. That's because practices like that lead to phenomena such as freshwater pollution, eutrophication, bioaccumulation and loss of aquatic organisms (Ojewole et al., 2024). For example, in Indonesia, 81.25% of wastewater generated by 16 fishery industries is discharged into water bodies without prior treatment (Ariyunita and Listyawati, 2020), whereas in the peruvian context, only about 32% of effluents produced nationwide are treated (Environmental Assessment and Enforcement Agency [OEFA], 2014)

One of the most widely used alternatives for reducing pollutant loads in fishery effluents is coagulation-flocculation as a primary treatment method (Land et al., 2020). That process occurs in two successive stages: coagulation, which involves the addition of one or more chemical or natural coagulants to destabilize suspended, dissolved or colloidal matter, and flocculation, in which particles aggregate to facilitate their removal (Sheng et al., 2022). Among the most used chemical coagulants, ferric chloride stands out due to its high efficacy in reducing turbidity, phosphorus (P), TSS and TDS (Ettaloui et al., 2021). However, its application presents certain drawbacks such as acidification (Winfield et al., 2016), sludge generation with high metal content (Koul et al., 2022) and environmental contamination due to the formation of toxic residues.

In response to those limitations, there is growing interest in the use of natural coagulants, which are positioned as more sustainable alternatives compared to chemical coagulants. Among natural coagulants, Moringa oleifera seeds powder - hereafter referred to as Moringa - and chitosan are noteworthy. On the one hand, Moringa seeds contain cationic proteins that act as coagulant agents, facilitating charge neutralization and particle aggregation, which contributes to reduce turbidity, biochemical oxygen demand (BOD), chemical oxygen demand (COD), TSS and TDS (Belbali et al., 2023). Chitosan, on the other hand, contains amino groups that impart high adsorption and flocculation abilities, thus effectively reducing those parameters (Yang et al., 2016). In that context, the present study aims to evaluate the efficacy of natural coagulants, such as chitosan and Moringa seeds powder, in comparison with ferric chloride (a chemical coagulant) for reducing TDS in wastewater from the Pucusana DPA, located in Lima, Peru.

### **MATERIALS AND METHODS**

# **Acquisition of coagulants**

The chitosan was supplied by AGRYLAAP S.A.C.S. company through its supplier Qingdao Habón Fertilizer Co. Ltd., while the ferric chloride was provided by Peruvian University of Applied Sciences after being obtained from Grupo Grat S.A.C. In turn, mature Moringa seeds were purchased to remove their shells manually and process them according to the series of steps followed by Desta and Bote (2021). In that sense, first, the seeds were ground into a fine powder, which was dried in an oven at 105 °C for 3 h after a pretreatment at 55 °C for 30 min and finally, sieved to ensure uniform particle size.

# Preparation of coagulant solutions

To prepare the chitosan solution, 3 g of the biopolymer were dissolved in 96 mL of distilled water and 1 mL of 1% acetic acid, maintaining continuous stirring at 500 rpm at 25 °C for 1 h (Ariffin et al., 2009). To obtain the Moringa seeds powder solution, 5 g of seed powder were diluted in 100 mL of distilled water with constant stirring at 500 rpm at 25 °C for 30 min (Fagundes-Klen et al., 2023). Finally, to prepare the ferric chloride solution, 1 g of the compound was dissolved in 100 mL of distilled water, maintaining continuous stirring at 375 rpm at 25 °C for 10 min (Chen et al., 2023). The coagulant solutions used in the study are shown in Figure 1.

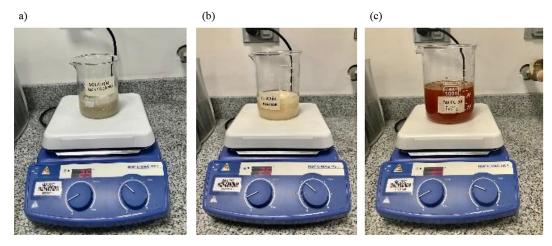


Figure 1. Coagulant solutions of (a) chitosan, (b) Moringa seeds powder and (c) ferric chloride

# Collection and characterization of sewage

Wastewater samples were collected at the Pucusana DPA, Lima, Peru, specifically at the outlet of the operational area where the discharge from the processing of hydrobiological resources is concentrated. First, 3 simple samples of 7 L each were taken between 4:00 a.m. and 5:00 a.m., a period of peak operational activity and consequently, higher effluent volume. Each simple sample was placed in a sterile container forming a composite sample representative of DPA's operations, which was homogenized by manual stirring for 5 min and stored again in the containers used for its collection. Each container was properly labeled with an identification code, date, time and sampling location. In addition, the samples were preserved at approximately 4 °C using refrigerants and transported to the water and renewable energy laboratory at the UPC within a period of no more than 6 h to ensure the integrity of each sample. The collection, preservation and handling of the samples were carried out following and adapting the guidelines established in the National Protocol for the Monitoring of the Quality of Surface Water Resources (National Water Authority [ANA] & Ministry of Agrarian Development and Irrigation [MIDAGRI], 2016), thereby ensuring the reliability of the results.

### **Experimental design**

The design to evaluate the influence of dose and type of coagulant on TDS reduction was completely randomized with a factorial arrangement, considering dose and coagulant type as factors A and B, with a and b levels respectively

for the response variable. Factor A, referring to dose, included 3 variants: chitosan, Moringa seeds powder and ferric chloride. Factor B, corresponding to coagulant type, was also analyzed considering 3 levels: 80 mg/0.5 L, 120 mg/0.5 L and 160 mg/0.5 L. Table 1 summarizes the levels established for each defined factor.

Similarly, the factorial design was structured based on the basic principles of experimental design. First, to comply with the principle of replication, the number of replicates per treatment was determined through a power analysis in the statistical software MINITAB (version 21.4, 64-bit). In that regard, 3 levels per factor were considered based on previous studies, where it is common to evaluate low, medium and high doses in addition to the coagulants under study (Karnena et al., 2022; Singh and Kumar, 2020). Also, a 0.05 significance level was established as the standard and 0.8 was set as the acceptable statistical power for a hypothesis test to be effective (Triola, 2018). Likewise, a maximum difference between means of 20 was assumed, considering that the parameter is set by the same author (Gutierrez and De la Vara, 2012) and a standard deviation of 1.03 was estimated based on studies conducted under similar conditions (Singh and Kumar, 2020; Sulistyowati et al., 2023; Worku and Abate, 2025). The result indicated a minimum of 2 replicates per treatment; however, 3 replicates were chosen to increase the reliability of the results and strengthen the statistical analysis (Jones and Montgomery, 2020). Second, to ensure the randomization of the experiments, the random function of Microsoft Excel (version 2401) was used to establish the execution order of the 30 experimental runs, resulting from a 3 × 3 factorial design involving 3 replicates per treatment and 3 controls. The random distribution of treatments is shown in Table 2. Finally, to comply with the principle of blocking, mixing speeds and times as well as sedimentation period for coagulation-flocculation were fixed to reduce their influence on the response variable. Rapid mixing is performed at high speeds and for short durations to promote the initial dispersion of the coagulant in the water, ensuring its efficient interaction with TSS (Ghernaout and Boucherit, 2015). In contrast, slow mixing is carried out at low speeds and over longer periods to facilitate floc formation (Al-Risheq et al., 2022). In addition, fixing the sedimentation time allows for effective settling of the flocs (Bhagavatula et al., 2021). In that way, each experimental run was conducted under homogeneous operating conditions to ensure comparability of results among the different treatments.

# **Experimental procedure**

Figure 2 shows the simulation of the coagulation-flocculation method using a jar test apparatus (PEF, EDIBON). The tests were conducted in 1 L beakers, to which 500 mL of the composite effluent sample and the corresponding coagulant dose were added. The operating conditions for each test sequence were 150 rpm for 2 min as rapid mixing, followed by 40 rpm for 30 min as slow mixing, and subsequently 30 min as the sedimentation time. Those periods were established after a review of previous studies related to the treatment of fishery effluents, which demonstrated the adequate formation and sedimentation of flocs through the sequence of times and mixing speeds considered in this study (Iber et al., 2023a, 2023b, 2023c). First, the rapid mixing time ensures the proper dispersion and contact of the coagulant with colloidal particles, facilitating charge destabilization (Ramphal and Sibiya, 2014). Subsequently, the slow mixing time allows already destabilized particles to collide and

Table 1. Levels of the factors studied

| Factor            | Code | Level         |  |
|-------------------|------|---------------|--|
| Dosage (mg/0.5 L) | А    | 80, 120 y 160 |  |
| Type of coagulant | В    | NC1, NC2 y CC |  |

**Note:** Chitosan was classified as natural coagulant 1 (NC1), Moringa seeds powder as natural coagulant 2 (NC2), and ferric chloride as chemical coagulant (CC).

aggregate (Lin et al., 2013). Finally, according to Costa and Fioravante (2024), the sedimentation time provides an appropriate balance between solids removal and practical process operation, thus reducing TDS.

# **Response variables**

For the estimation of TDS reduction after the application of the treatments, 20 mL of sample was extracted from each beaker using a volumetric pipette positioned 3 cm below the surface

**Table 2.** Randomized trial sequence of the experimental runs

| Trial    | Trial Experimental |          | tment    |  |
|----------|--------------------|----------|----------|--|
| sequence | run number         | Factor A | Factor B |  |
| 1        | 20                 | 160      | NC2      |  |
| 2        | 1                  | 0        | ND       |  |
| 3        | 19                 | 160      | NC2      |  |
| 4        | 24                 | 80       | CC       |  |
| 5        | 14                 | 80       | NC2      |  |
| 6        | 27                 | 120      | CC       |  |
| 7        | 15                 | 80       | NC2      |  |
| 8        | 7                  | 120      | NC1      |  |
| 9        | 13                 | 80       | NC2      |  |
| 10       | 22                 | 80       | CC       |  |
| 11       | 4                  | 80       | NC1      |  |
| 12       | 10                 | 160      | NC1      |  |
| 13       | 17                 | 120      | NC2      |  |
| 14       | 2                  | 0        | ND       |  |
| 15       | 26                 | 120      | CC       |  |
| 16       | 3                  | 0        | ND       |  |
| 17       | 12                 | 160      | NC1      |  |
| 18       | 21                 | 160      | NC2      |  |
| 19       | 6                  | 80       | NC1      |  |
| 20       | 25                 | 120      | CC       |  |
| 21       | 11                 | 160      | NC1      |  |
| 22       | 28                 | 160      | CC       |  |
| 23       | 8                  | 120      | NC1      |  |
| 24       | 30                 | 160      | СС       |  |
| 25       | 9                  | 120      | NC1      |  |
| 26       | 29                 | 160      | CC       |  |
| 27       | 5                  | 80       | NC1      |  |
| 28       | 16                 | 120      | NC2      |  |
| 29       | 18                 | 120      | NC2      |  |
| 30       | 23                 | 80       | CC       |  |

**Note:** A value of 0 in factor A and ND (Not Defined) in factor B correspond to the control conditions (beakers without treatment).

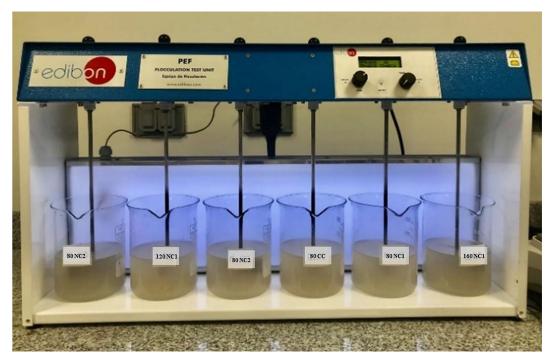


Figure 2. Simulation of the coagulation/flocculation method using jar tests

(Chen et al., 2023). The percentage of TDS reduction was calculated based on Equation 1.

Removal rate (%) = 
$$\left(\frac{Ci-Cf}{Ci}\right) \times 100$$
 (1)

where: *Ci* and *Cf* represent the initial and final concentrations respectively for the parameter under study.

# Statistical analysis

Since the proposed design was factorial, the statistical analysis was a two-way analysis of variance (ANOVA) with a significance level of 5% ( $\alpha = 0.05$ ) to statistically assess whether the dose and type of coagulant influence TDS reduction. It should be noted that before performing the ANOVA, its assumptions were verified, namely normality, homogeneity of variances and error independence (Hernández et al., 2014).

Likewise, to validate the experimental design, compliance with its basic principles was ensured, while, based on the factorial design, a mathematical model was established to describe the relationship between the factors and the analyzed response variable.

In the same manner, multiple comparison tests were performed using Tukey's method with a 95% confidence level to identify the most

effective treatments as well as those which differ significantly from each other.

Additionally, 95% confidence intervals were determined for the meaning of each treatment to narrow the range in which the true population value is likely to be found. Furthermore, from the lower and upper limits of each interval, the error margin was calculated through the half-difference of its extremes for each treatment (Hazra, 2017).

The data analysis as well as the tabular and graphical representation of the results was carried out using MINITAB software version 21.4 (64-bit) and Microsoft Excel 2401, respectively.

### **RESULTS AND DISCUSSION**

Physicochemical characteristics of the sewage

Physicochemical parameters such as pH, turbidity, COD, TSS and TDS are crucial indicators for establishing water quality (Sulistyowati et al., 2024). Therefore, the concentration of TDS in wastewater generated by the Pucusana DPA was studied. Table 3 shows the initial quality of the effluent in terms of TDS and pH using a conductivity meter and a pH meter, respectively. Regarding its TDS concentration (82.7  $\pm$  1.62 mg/0.5 L), it is important to highlight that it is a relatively low value, like the one obtained by Das et al.

**Table 3.** Physicochemical characteristics of the sewage

| Parameter | Unit     | Value       |
|-----------|----------|-------------|
| TDS       | mg/0.5 L | 82.7 ± 1.62 |
| pН        | pH unit  | 6.8 ± 0.25  |

(2023). In turn, its pH value ( $6.8 \pm 0.25$ ) shows a slight tendency towards alkalinity despite having been affected by factors such as temperature and decomposition of organic matter in the water (Olaoluwa et al., 2024).

# Effect of parameters studied on TDS reduction

The interaction of the factors in the TDS reduction is shown in Figure 3 and validated by the p-value obtained (0.00), which is lower than the significance level considered (0.05), according to the significance test that will be detailed as part of the statistical results. Based on Figure 3, there is an interaction effect between the dose and the type of coagulant, since the straight-line segments symbolizing the doses of 80 mg/0.5 L, 120 mg/0.5 L and 160 mg/0.5 L intersect. Likewise, the straightline segments representing the dose of 160 mg/0.5 L are located at a higher position than the straightline segments corresponding to the doses of 80 mg/0.5 L and 120 mg/0.5 L. Therefore, it is evident that at a dose of 160 mg/0.5 L, the TDS reduction is usually greater. About chitosan, it is noteworthy that it generated reductions of up to approximately

98%. Specifically, doses of 80 mg/0.5 L, 120 mg/0.5 L, and 160 mg/0.5 L reduced the presence of TDS by  $84.16 \pm 0.80\%$ ,  $95.08 \pm 1.49\%$  and  $98 \pm$ 0.71%, respectively. In other words, the efficacy of chitosan increased as the dose increased. That behavior coincides with the findings of Sulistyowati et al. (2024), who indicate that as the chitosan dose increases, the TDS concentration decreases. In agreement with Muniz et al. (2022), chitosan, a branched nuclear polymer, can absorb onto the active sites of colloids, causing their destabilization and therefore, the formation of agglomerates that easily sediment or float. In that sense, the proportional relationship identified is because as the dose increases, a larger number of branches that can remove TDS predominate. However, Chen et al. (2023) note that chitosan overdosing can cause a reversal in the surface charge of the particles, which would increase their concentration and decrease their capacity as a coagulant.

Similarly, the application of Moringa seed powder doses reduced the presence of TDS by up to approximately 87%, which is lower than the maximum reduction obtained after the use of chitosan. Specifically, the addition of 80 mg/0.5 L, 120 mg/0.5 L and 160 mg/0.5 L as doses in the effluent samples produced reductions of  $70.98 \pm 2.09\%$ ,  $79.26 \pm 1.17\%$  and  $86.98 \pm 1.92\%$ , respectively. To put it another way, it was observed that the TDS reduction increased in parallel with the dose, like chitosan works, as reported by Ogunshina et al. (2023). That efficacy was attributed to

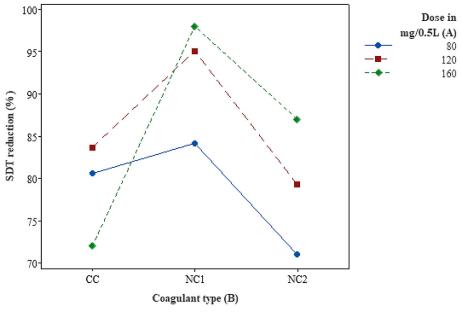


Figure 3. Interaction plot for TDS reduction

the composition of Moringa seeds, as they contain low molecular weight, water-soluble cationic proteins that interact with the organic material in the effluent, causing its instability and thus facilitating its removal by sedimentation (Hadadi et al., 2022; Souza et al., 2021). In other words, the direct relationship observed can be explained by the fact that higher doses contain a higher content of active proteins capable of reducing particle concentration. Nevertheless, it is important to emphasize as a possible environmental limitation that an overdose of Moringa seed powder can promote the generation of organic matter in the treated effluent, which contributes to the formation of carcinogenic trihalomethanes if the organic matter comes into contact with chlorine during a disinfection process (Diver et al., 2023).

Finally, the chemical coagulant, ferric chloride, produced reductions of up to 84%. Specifically, the dose of 80 mg/0.5 L produced a decrease of  $80.57 \pm 0.5\%$ , a percentage that increased to  $83.64 \pm 0.14\%$  with a dose of 120 mg/0.5 L but decreased to  $71.95 \pm 0.5\%$  with a dose of 160 mg/0.5 L. That behavior is like the one obtained by Singh and Kumar (2020), who showed that the TDS reduction using ferric chloride partially decreased with increasing dose. That tendency according to the cited authors could be explained by the phenomena of adsorption and/or sweep flocculation, since a saturated adsorbent surface immediately loses its ability to retain more contaminants, while very dense flocs settle so quickly that they fail to adequately capture the finer particles. In addition, that behavior is explicated because chemical coagulants perform better at maximum pH levels but high doses of ferric chloride in this case tend to significantly decrease the pH of the effluent (Liu et al., 2024; Singh and Kumar, 2020). However, given that those percentages are above 50%, Karnena et al. (2022) highlight its efficacy, which is facilitated by the solubility of ferric hydroxide at high ionic strength.

To sum up, the dose and type of coagulant influence the TDS reduction as shown in Table 4, because natural coagulants produce greater decreases compared to chemical coagulants at higher doses. Specifically, chitosan produced the greatest reduction (98  $\pm$  0.71%) at a dose of 160 mg/0.5 L, followed by Moringa seeds powder (86.98  $\pm$  1.92%) also at a dose of 160 mg/0.5 L and ferric chloride (83.64  $\pm$  0.14%) at a dose of 120 mg/0.5 L. In that regard, it was demonstrated that natural coagulants improved their efficacy as their doses increased.

However, that behavior was due to the pH level of effluent, since natural coagulants perform better in near-alkaline conditions (Jaganathan et al., 2022; Nouj et al., 2021). In addition, that type of coagulant is cost-effective, since its low-cost acquisition generates effective results and in turn sustainable, since it does not produce large amounts of non-biodegradable sludge or alter the pH level of water bodies, compared to chemical coagulants (Desta and Bote, 2021; Kurniawan et al., 2021; Wagh et al., 2022). Therefore, currently, its use is being studied for the treatment of various sources of wastewater.

# Statistical analysis

### Validation of the experimental design

The experimental design was structured in accordance with its fundamental principles. The principles of replication and randomization were satisfied by conducting each treatment up to three times, following the randomization scheme presented in Table 2. Furthermore, the principle of blocking was addressed by controlling mixing speeds and times, as well as the sedimentation period in each test sequence, since these operating conditions may influence the efficacy of the observed response variable.

# Development of the mathematical model equation

The equation of the mathematical model based on the factorial design is depicted in Equation 2:

$$y_{ijk} = \mu + \tau_i + \beta_i + (\tau \beta)_{ij} + \varepsilon_{ijk}$$
 (2)

$$i = 1, 2, 3 = a$$
;  $j = 1, 2 = b$ ;  $k = 1, 2, 3 = n$ 

where:  $\mu$  – global average effect,  $\tau_i$  – effect of the i-th level of the factor A,  $\beta_j$  – effect of the j-th level of the factor B,  $(\tau\beta)_{ij}$  – interaction effect between the factors,  $\varepsilon_{ijk}$  – random error with a normal distribution that has a mean of zero and constant variance; that error is also linked to  $y_{ijk}$ , representing the k-th half-liter of the sewage where the i-th dose of the j-th type of coagulant is applied.

### Analysis of variance - ANOVA

ANOVA is a technique that is used to assess the impact of one or more factors and their interaction on one or more response variables (Jasim and Salman, 2024). Table 5 provides a summary of the findings obtained from the analysis. Based on those values, it was rejected that the interaction of

**Table 4.** TDS reduction according to the applied treatment

| Treatment         |     |                                | TDS in the sewa               | ge    |                 |  |
|-------------------|-----|--------------------------------|-------------------------------|-------|-----------------|--|
| Factor A Factor B |     | Before treatment<br>(mg/0.5 L) | After treatment<br>(mg/0.5 L) | TDS   | S reduction (%) |  |
|                   |     | 82.7                           | 12.83                         | 84.49 |                 |  |
| 80                | NC1 | 82.7                           | 13.36                         | 83.85 | 84.16 ± 0.8     |  |
|                   |     | 82.7                           | 13.12                         | 84.14 |                 |  |
|                   |     | 82.7                           | 4.25                          | 94.86 |                 |  |
| 120               | NC1 | 82.7                           | 3.51                          | 95.76 | 95.08 ± 1.49    |  |
|                   |     | 82.7                           | 4.45                          | 94.62 |                 |  |
|                   |     | 82.7                           | 1.70                          | 97.94 | 98 ± 0.71       |  |
| 160               | NC1 | 82.7                           | 1.40                          | 98.31 |                 |  |
|                   |     | 82.7                           | 1.86                          | 97.75 |                 |  |
|                   |     | 82.7                           | 23.55                         | 71.52 |                 |  |
| 80                | NC2 | 82.7                           | 23.65                         | 71.40 | 70.98 ± 2.09    |  |
|                   |     | 82.7                           | 24.80                         | 70.01 |                 |  |
|                   |     | 82.7                           | 17.45                         | 78.90 |                 |  |
| 120               | NC2 | 82.7                           | 17.30                         | 79.08 | 79.26 ± 1.17    |  |
|                   |     | 82.7                           | 16.71                         | 79.79 |                 |  |
| 160 N             |     | 82.7                           | 10.94                         | 86.77 |                 |  |
|                   | NC2 | 82.7                           | 10.06                         | 87.84 | 86.98 ± 1.92    |  |
|                   |     | 82.7                           | 11.30                         | 86.34 |                 |  |
|                   |     | 82.7                           | 15.87                         | 80.81 |                 |  |
| 80                | CC  | 82.7                           | 16.15                         | 80.47 | 80.57 ± 0.51    |  |
|                   |     | 82.7                           | 16.18                         | 80.44 |                 |  |
|                   |     | 82.7                           | 13.57                         | 83.59 |                 |  |
| 120               | CC  | 82.7                           | 13.48                         | 83.70 | 83.64 ± 0.14    |  |
|                   |     | 82.7                           | 13.53                         | 83.64 |                 |  |
|                   |     | 82.7                           | 23.30                         | 71.83 |                 |  |
| 160               | CC  | 82.7                           | 23.00                         | 72.19 | 71.95 ± 0.5     |  |
|                   |     | 82.7                           | 23.28                         | 71.85 |                 |  |

factors has no influence on the TDS reduction. In other words, it was assumed that it had an impact, because the p-value obtained (0.00) was lower than the significance level considered (0.05) in the criterion for rejection and non-rejection of  $H_0$ .

It should be emphasized that the fulfillment of its assumptions is reflected in the p-values obtained through the Normality Test (Anderson-Darling) and Homogeneity of Variance Test (Bartlett) for the assumption of normality and homogeneity of variances, respectively. Specifically, the p-values for the first and second assumptions mentioned were 0.43 and 0.13, respectively, which are greater than the preestablished significance level (0.05). Likewise, the assumption of error independence was also fulfilled, as only random behavior patterns were observed in Figure 4.

### Tukey's HSD (honestly significant difference)

Table 6 displays the results of the multiple range tests using Tukey's method with a 95% confidence level. Based on that, the most effective treatments were those involving the application of natural coagulants at generally higher doses, as they yielded higher mean values and belonged to only one group due to significant difference. In contrast, treatments with ferric chloride at doses of 120 mg/0.5 L, 80 mg/0.5 L and 160 mg/0.5 L didn't differ significantly from those with chitosan at 80 mg/0.5 L or Moringa seeds powder at 120 mg/0.5 L and 80 mg/0.5 L, respectively. Figure 5 displays the visual differences or absence of differences between the reduction percentages obtained after applying the treatments to the effluent samples.

Table 5. ANOVA results for TDS reduction

| Source                                    | DF | Adj SS  | Adj MS | F-value | P-value |
|---|----|---------|--------|---------|---------|
| Dose in mg/0.5 L (A)                      | 2  | 315.92  | 157.96 | 660.08  | 0.00    |
| Coagulant type (B)                        | 2  | 1096.48 | 548.24 | 2291.01 | 0.00    |
| Dose in mg/0.5 L (A) × coagulant type (B) | 4  | 608.13  | 152.03 | 635.32  | 0.00    |
| Error                                     | 18 | 4.31    | 0.24   |         |         |
| Total                                     | 26 | 2024.82 |        |         |         |

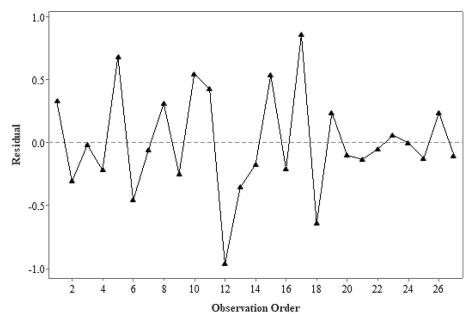


Figure 4. Residual vs order

# Comparison of the maximum reduction of TDS with literature values

Table 7 illustrates the results of previous studies, in addition to those obtained in the present study. Based on the results of this investigation, the application of coagulants to reduce TDS is promising, because they generated removals greater than 50%. Likewise, compared to the results of

other studies, it was observed that the reduction percentages achieved are optimistic due to the favorable conditions of the effluent, for example, its initial TDS concentration and pH level, limiting factors in the efficacy of TDS reduction (Diver et al., 2023). According to Bhagavath and Subrahmanian (2025), the high presence of TDS tends to alter the density of wastewater and therefore, reduce the efficacy of coagulation-flocculation by

**Table 6.** Tukey's pairwise comparisons

| Dose in mg/0.5 L (A) × coagulant type (B) | N | Mean  | Grouping |   |   |   |   |   |
|---|---|-------|----------|---|---|---|---|---|
| 160 NC1                                   | 3 | 98.00 | А        |   |   |   |   |   |
| 120 NC1                                   | 3 | 95.08 |          | В |   |   |   |   |
| 160 NC2                                   | 3 | 86.98 |          |   | С |   |   |   |
| 80 NC1                                    | 3 | 84.16 |          |   |   | D |   |   |
| 120 CC                                    | 3 | 83.64 |          |   |   | D |   |   |
| 80 CC                                     | 3 | 80.57 |          |   |   |   | E |   |
| 120 NC2                                   | 3 | 79.26 |          |   |   |   | E |   |
| 160 CC                                    | 3 | 71.96 |          |   |   |   |   | F |
| 80 NC2                                    | 3 | 70.98 |          |   |   |   |   | F |

Note: Means that do not share a letter are significantly different.

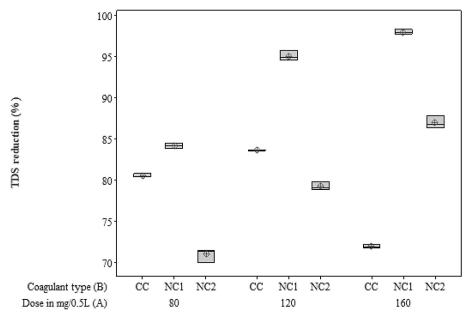


Figure 5. Boxplot of TDS reduction

**Table 7.** Results of the present study, with some previous studies

| Sewage before treatment |       | Treatment            |              | TDC reduction (0/) | Reference                   |  |
|-------------------------|-------|----------------------|--------------|--------------------|-----------------------------|--|
| TDS                     | рН    | Coagulant            | Dose         | TDS reduction (%)  | Releience                   |  |
| 82.7 mg/0.5 L           | 6.8   |                      | 160 mg/0.5 L | 98 ± 0.71%         | This study                  |  |
| 16.064 mg/L             | 7.32  | Chitosan             | 80 mg/L      | 81.49%             | (Sulistyowati et al., 2023) |  |
| 80.8 g/L                | 7.8   | Chilosan             | 0.20 g/L     | 79%                | (Das et al., 2023)          |  |
| 6.480 mg/L              | 9.02  |                      | 0.5 g/100 mL | 66%                | (Al Ajmi et al., 2023)      |  |
| 82.7 mg/0.5 L           | 6.8   |                      | 160 mg/0.5 L | 86.98 ± 1.92%      | This study                  |  |
| 4.000 mg/L              | 8.5   | Moringa seeds powder | 5 mg/L       | 75.8%              | (Worku and Abate, 2025)     |  |
| 3.256 mg/L              | 11.65 | powdor               | 80 mL        | 63.2%              | (Balaji et al., 2018)       |  |
| 82.7 mg/0.5 L           | 6.8   | F : 11 :12           | 120 mg/0.5 L | 83.64 ± 0.14%      | This study                  |  |
| 4.761 mg/L              | 7     | Ferric chloride      | 0.20 g/L     | 93.68%             | (Singh and Kumar, 2020)     |  |

hindering the sedimentation of particles. That's why TDS reductions in this study were greater than those in the other studies. In the same way, natural coagulants were found to perform better under near-alkaline conditions, since the TDS reductions in this study were higher than those in the other studies, which had effluents with predominantly alkaline pH levels (Jaganathan et al., 2022; Nouj et al., 2021). Additionally, as reported by Singh and Kumar (2020), the optimal TDS reduction after applying chemical coagulants occurs at a maximum pH level and a minimum coagulant dose. In other words, the TDS reduction increases with increasing pH but decreases with increasing dose. That's why the percentage referring to the application of ferric chloride in this study is lower than the percentage obtained by the cited authors.

#### CONCLUSIONS

The study demonstrated that the coagulants performed remarkably well in reducing TDS in the wastewater of DPA Pucusana, as they achieved reductions greater than 70% in all treatments. The highest reductions were achieved specifically with chitosan at doses of 160 mg/0.5 L (98  $\pm$  0.71%) and 120 mg/0.5 L (95.08  $\pm$  1.49%), followed by Moringa seeds powder at a dose of 160 mg/0.5 L (86.98  $\pm$  1.92%). In that regard, the results indicate that natural coagulants proved to be more effective than ferric chloride, which decreased its performance at higher doses, although it is essential to keep in mind that natural coagulants require a near-alkaline pH level to generate those high percentages. In summary, the findings

support natural coagulants as a viable alternative for the treatment of wastewater from the fishing sector, as they are effective and have positive environmental impacts.

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### **REFERENCES**

- Al Ajmi, S., Ali Syed, M., Shaik, F., Nayeemuddin, M., Balakrishnan, D., Myneni, V. (2023). Treatment of industrial saline wastewater using eco-friendly adsorbents. *Journal of Chemistry*, 2023, 1–11. https://doi.org/10.1155/2023/7366941
- 2. Al-Dawery, S., AL-Yaqoubi, G., Al-Musharrafi, A., Harharah, H., Amari, A., Harharah, R. (2023). Treatment of fish-processing wastewater using polyelectrolyte and palm anguish. *Processes*, *11*(7), 1–14. https://doi.org/10.3390/pr11072124
- 3. Al-Risheq, D. I. M., Shaikh, S. M. R., Nasser, M. S., Almomani, F., Hussein, I. A., Hassan, M. K. (2022). Enhancing the flocculation of stable bentonite suspension using a hybrid system of polyelectrolytes and NADES. Colloids and Surfaces A: *Physicochemical and Engineering Aspects*, 638(1), 1–13. https://doi.org/10.1016/j.colsurfa.2022.128305
- Anh, H., Shahsavari, E., Bott, N., Ball, A. (2021). The application of Marinobacter hydrocarbonoclasticus as a bioaugmentation agent for the enhanced treatment of non-sterile fish wastewater. *Journal of Environmental Management*, 291(1), 1–8. https://doi.org/10.1016/j.jenvman.2021.112658
- 5. Ariffin, M., Pei, T., Zainon, Z. (2009). Coagulation and flocculation treatment of wastewater in textile industry using chitosan. *Journal of Chemical and Natural Resources Engineering*, *4*(1), 43–53. https://n9.cl/qj8vw7
- 6. Ariyunita, S., Listyawati, R. (2020). Mapping the potential pollution of fisheries industry wastewater in the Southern Coast of Jember Regency: Preliminary study on wastewater management planning. *Journal of Physics: Conference Series*, 1465(1), 1–9.

- https://doi.org/10.1088/1742-6596/1465/1/012004
- Ayyoub, H., Kitanou, S., Bachiri, B., Tahaikt, M., Taky, M., Elmidaoui, A. (2022). Membrane bioreactor (MBR) performance in fish canning industrial wastewater treatment. *Water Practice and Technology*, 17(6), 1358–1368. https://doi.org/10.2166/wpt.2022.059
- 8. Balaji, V., Kumar, S., Ashwin, R. (2018). Industrial effluent treatment by *Moringa Oleifera* as a natural coagulant for different particle sizes. *Asian Journal of Microbiology Biotechnology and Environmental Sciences*, 20(2), 550–556. https://www.researchgate.net/publication/326081082
- Belbali, A., Benghalem, A., Gouttal, K., Taleb, S. (2023). Coagulation of turbid wastewater with an active component extracted from Moringa oleifera seeds. *International Journal of Environmental Analytical Chemistry*, 103(20), 8689–8705. https://doi. org/10.1080/03067319.2021.1995725
- Bhagavath, R., Subrahmanian, S. (2025). Utilizing green biomaterials for reducing total dissolved solids: a sustainable approach to industrial effluent treatment. *Asian Journal of Green Chemistry*, 9(2), 208–219. https://doi.org/10.48309/AJGC.2025.492947.1609
- Bhagavatula, A., Rajagopalan, V., Duncan, B., Vimalchand, P. (2021). Innovative recovered water process implementation: Flocculation-sedimentation-filtration process for addressing water and energy nexus challenges at Kemper IGCC Power Plant. *Energy Nexus 1*(1), 1–10. https://doi.org/10.1016/j.nexus.2021.100007
- Chen, T., Ismail, N., Oh, K., Tee, L. (2023). Coagulation-flocculation process for greywater treatment using Chitosan and Hibiscus Sabdariffa. *Journal of Physics: Conference Series*, 2523. https://doi.org/10.1088/1742-6596/2523/1/012013
- Costa, L., Fioravante, I. (2024). Evaluation the efficiency of individual organic coagulants and associated with aluminum sulfate in the removal of colloidal substances from Rio Doce, Minas Gerais, Brazil. Cleaner Chemical Engineering, 10(1), 100134. https://doi.org/10.1016/j.clce.2024.100134
- 14. Das, N., Rajput, H., Aly Hassan, A., Kumar, S. (2023). Application of different coagulants and cost evaluation for the treatment of oil and gas produced water. *Water*, *15*(3), 464. https://doi.org/10.3390/w15030464
- 15. Desta, W., Bote, M. (2021). Wastewater treatment using a natural coagulant (*Moringa oleifera* seeds): optimization through response surface methodology. *Heliyon*, 7(11). https://doi.org/10.1016/j.heliyon.2021.e08451
- 16. Diver, D., Nhapi, I., Rutendo, W. (2023). The potential and constraints of replacing conventional chemical coagulants with natural plant extracts in water

- and wastewater treatment. *Environmental Advances*, 13. https://doi.org/10.1016/j.envadv.2023.100421
- 17. Environmental Assessment and Enforcement Agency (OEFA). (2014). The OEFA warns of environmental problems due to a lack of wastewater treatment at the national level (in Spanish). https://www.gob.pe/institucion/oefa/noticias/20794-el-oefa-advierte-problematica-ambiental-por-deficit-de-tratamiento-de-las-aguas-residuales-a-nivel-nacional
- 18. Ettaloui, Z., Salah, S., Aguelmous, A., Jada, A., Taleb, A. (2021). Use of ferric chloride contained in the rejects from the steel industry as a coagulant for the fuel washing wastewater treatment. *Desalination and Water Treatment*, 234(1), 68–76. https://doi.org/10.5004/dwt.2021.27556
- 19. Fagundes-Klen, M., Gullich, C., Triques, C., Formentini-Schmitt, D., Veit, M., Bergamasco. (2023). Valorization of the coagulant bioactive compound of the moringa seed residue: Treatability of fish processing residuary waters. Waste and Biomass Valorization, 14(12), 4113–4126. https://doi.org/10.1007/s12649-023-02110-x
- 20. Food and Agriculture Organization (FAO). (2016). *Sustainable artisanal fishing* (in Spanish). https://www.fao.org/policy-support/policy-themes/sustainable-small-scale-fisheries/es
- 21. Ghernaout, D., Boucherit, A. (2015). Review of coagulation's rapid mixing for NOM removal. *Journal of Research & Developments in Chemistry*, 2015(1). 1–32. https://doi.org/10.5171/2015.926518
- 22. González, R., Narvarte, M., Arias, M., Avaca, S., Crespo, E. (2025). Impact of fisheries on marine ecosystems. *In Marine Ecology*, 2(1), 60–78. CRC Press. https://doi.org/10.1201/9781003024613-3
- 23. Gutiérrez, H., De la Vara, R. (2012). *Analysis and Experimental Design*. (3ª ed.). McGraw-Hill (in Spanish). https://www.academia.edu/32094439/An%C3%A1lisis\_y\_dise%C3%B1os\_de\_experimentos\_3ra\_edici%C3%B3n\_Gutierrez\_Pulido\_pdf
- 24. Hadadi, A., Imessaoudene, A., Bollinger, J.-C., Assadi, A., Amrane, A., Mouni, L. (2022). Comparison of four plant-based bio-coagulants performances against alum and ferric chloride in the turbidity improvement of bentonite synthetic water. *Water*, *14*(20). https://doi.org/10.3390/w14203324
- 25. Hazra, A. (2017). Using the confidence interval confidently. *Journal of Thoracic Disease*, *9*(10), 4125–4130. https://doi.org/10.21037/jtd.2017.09.14
- 26. Hernández, R., Fernández, C., Baptista, P. (2014). *Research Methodology.* (6<sup>a</sup> ed.). McGraw-Hill Spain (in Spanish). https://dialnet.unirioja.es/servlet/libro?codigo=775008
- 27. Iber, B., Torsabo, D., Chik, C., Wahab, F., Abdullah, S., Hasan, H., Kasan, N. (2023a). A study on the

- recovery and characterization of suspended solid from aquaculture wastewater through coagulation/flocculation using chitosan and its viability as organic fertilizer. *Journal of Agriculture and Food Research*, *11*(1), 1–12. https://doi.org/10.1016/j.jafr.2023.100532
- 28. Iber, B., Torsabo, D., Chik, C., Wahab, F., Abdullah, S., Hasan, H., Kasan, N. (2023b). Optimization of chitosan coagulant from dry legs of giant freshwater prawn, *Macrobrachium rosenbergii* in aquaculture wastewater treatment using response surface methodology (RSM). *Journal of Environmental Chemical Engineering*, 11(3), 1–16. https://doi.org/10.1016/j.jece.2023.109761
- Iber, B., Torsabo, D., Chik, C., Wahab, F., Abdullah, S., Hasan, H., Kasan, N. (2023c). Response surface methodology (RSM) approach to optimization of coagulation-flocculation of aquaculture wastewater treatment using chitosan from carapace of giant freshwater prawn Macrobrachium Rosenberger. *Polymers*, 15(4), 1–23. https://doi.org/10.3390/polym15041058
- Jaganathan, J., Abdullah, S., Ismail, N., Sharuddin, S. (2022). Coagulation-flocculation process of nutrient-rich suspended solids from aquaculture effluent using bioflocculant. *Journal of Biochemistry, Microbiology and Biotechnology, 10*, 46–56. https://doi.org/10.54987/jobimb.v10isp2.728
- 31. Jasim, R., Salman, R. (2024). Use of nano coni-mn composite and aluminum for removal of artificial anionic dye congo red by combined system. *Ecological Engineering and Environmental Technology*, 25(7), 133–149. https://doi.org/10.12912/27197050/188266
- 32. Jones, B., Montgomery, D. (2020). *Design of Experiments: A Modern Approach*. John Wiley & Sons. Inchttps://www.buscalibre.com/int-es/libro-design-of-experiments-a-modern-approach/978111974601 0/p/53330263
- 33. Karnena, M., Konni, M., Dwarapureddi, B., Saritha, V. (2022). Blend of natural coagulants as a sustainable solution for the challenges of pollution from aquaculture wastewater. *Applied Water Science*, *12*(3), 1–14. https://doi.org/10.1007/s13201-021-01501-6
- 34. Koul, B., Bhat, N., Abubakar, M., Mishra, M., Arukha, A. P., Yadav, D. (2022). Application of natural coagulants in water treatment: a sustainable alternative to chemicals. *Water*, *14*(22), 1–27. https://doi.org/10.3390/w14223751
- 35. Kurniawan, S., Abdullah, S., Othman, A., Purwanti, I., Imron, M., Ismail, N., Ahmad, A., Hasan, H. (2021). Isolation and characterisation of bioflocculant-producing bacteria from aquaculture effluent and its performance in treating high turbid water. *Journal of Water Process Engineering*, 42. https://

- doi.org/10.1016/j.jwpe.2021.102194
- 36. Kusumanti, I., Yulianti, W., Jannah, N. (2021). Physiochemical property of wastewater discharged from smoked fish industry around fish-ponds area in Penatarsewu Village, Sidoardjo, East Java. *IOP Conference Series: Earth and Environmental Science*, 744(1), 012037. https://doi.org/10.1088/1755-1315/744/1/012037
- 37. Land, T., Veit, M., Da Cunha, G., Palácio, S., Barbieri, J., de Oliveira, C., Campos, E. (2020). Evaluation of a coagulation/flocculation process as the primary treatment of fish processing industry wastewater. *Water, Air, & Soil Pollution, 231*(9), 1–12. https://doi.org/10.1007/s11270-020-04811-8
- 38. Lin, J.-L., Pan, J., Huang, C. (2013). Enhanced particle destabilization and aggregation by flash-mixing coagulation for drinking water treatment. *Separation and Purification Technology*, *115*, 145–151. https://doi.org/10.1016/j.seppur.2013.05.013
- 39. Liu, W., Lyu, J., Wu, D., Cao, Y., Ma, Q., Lu, Y., Zhang, X. (2022). Cutting Techniques in the Fish Industry: A Critical Review. *Foods*, *11*(20), 1–23. https://doi.org/10.3390/foods11203206
- 40. Liu, M., Rashid, S., Wang, W., Zhang, H., Zhao, Y., Fu, X., Su, Z., Graham, N., Yu, W. (2024). The application of chitosan quaternary ammonium salt to replace polymeric aluminum ferric chloride for sewage sludge dewatering. *Water Research*, *256*. https://doi.org/10.1016/j.watres.2024.121539
- 41. Ministry of Production (PRODUCE). (2020). *PRODUCE: Artisanal fishing accounts for more than 64% of CHD's marine products (in Spanish)*. https://www.gob.pe/institucion/produce/noticias/189221-produce-pesca-artesanal-contribuye-con-masdel-64-de-productos-marinos-de-chd
- 42. Muniz, G., Borges, A., Da Silva, T., Batista, R., De Castro, S. (2022). Chemically enhanced primary treatment of dairy wastewater using chitosan obtained from shrimp wastes: optimization using a Doehlert matrix design. *Environmental Technology*, 43(2), 237–254. https://doi.org/10.1080/09593330.2020.1783372
- 43. National Water Authority (ANA), & Ministry of Agrarian Development and Irrigation (MIDAGRI). (2016). National Protocol for Monitoring the Quality of Surface Water Resources (in Spanish). https://sinia.minam.gob.pe/sites/default/files/siar-puno/archivos/public/docs/1475.pdf
- 44. Nouj, N., Hafid, N., El Alem, N., Cretescu, I. (2021). Novel Liquid Chitosan-Based Biocoagulant for Treatment Optimization of Fish Processing Wastewater from a Moroccan Plant. *Materials*, 14(23), 7133. https://doi.org/10.3390/ma14237133
- 45. Ogunshina, M., Abioye, O., Adeniran, K., Olasehinde, D. (2023). *Moringa Oleifera* Coagulation Characteristics in Wastewater Treatment in a University Dormitory. *Nature Environment and*

- *Pollution Technology, 22*(2), 699–707. https://doi.org/10.46488/NEPT.2023.v22i02.013
- 46. Ojewole, A., Ndimele, P., Oladele, A., Saba, A., Oladipupo, I., Ojewole, C., Ositimehin, K., Oluwasanmi, A., Kalejaye, O. (2024). Aquaculture wastewater management in Nigeria's fisheries industry for sustainable aquaculture practices. *Scientific African*, 25(1), 1–14. https://doi.org/10.1016/j.sciaf.2024.e02283
- 47. Olaoluwa, D., Owonibi, S., Hussain, R., Adenipekun, O., Salotun, R., Olufade, I., Adiele, G. (2024). Assessment of aquaculture wastewater impact on Osun River, Ede, Nigeria. *Proceedings of the Nigerian Society of Physical Sciences, 1*(1). https://doi.org/10.61298/pnspsc.2024.1.79
- 48. Pushpalatha, N., Sreeja, V., Karthik, R., Saravanan, G. (2022). Total Dissolved Solids and Their Removal Techniques. *International Journal of Environmental Sustainability and Protection*, 2(2), 13–20.
- 49. Ramphal, S., Sibiya, S. M. (2014). Optimization of Time Requirement for Rapid Mixing During Coagulation Using a Photometric Dispersion Analyzer. *Procedia Engineering*, 70, 1401–1410. https://doi.org/10.1016/j.proeng.2014.02.155
- 50. Ribeiro, J., Juarez, J. (2021). Phosphorus Removal Technology: Managing the Element in Industrial Waste. *Revista Ambiente e Agua*, *9*(3), 445–458 (in Portuguese). https://doi.org/10.4136/1980-993X
- 51. Sheng, D., Bilad, M., Shamsuddin, N. (2022). Assessment and Optimization of Coagulation Process in Water Treatment Plant: A Review. *ASEAN Journal of Science and Engineering*, *3*(1), 79–100. https://doi.org/10.17509/ajse.v3i1.45035
- 52. Singh, B., Kumar, P. (2020). Pre-treatment of petroleum refinery wastewater by coagulation and flocculation using mixed coagulant: Optimization of process parameters using response surface methodology (RSM). *Journal of Water Process Engineering*, *36*(1), 1–177. https://doi.org/10.1016/j.jwpe.2020.101317
- 53. Souza, B., Eyng, E., Baraldi, I., Frare, L., Pisano, G., Bergamasco, R., Fagundes-Klen, M., Ferreira Da Costa, P. (2021). Life performance evaluation of lyophilized Moringa biocoagulant: An alternative for prolonging the biocoagulant efficiency. *Environmental Progress and Sustainable Energy*, 40(3). https://doi.org/10.1002/ep.13538
- 54. Sulistyowati, L., Andareswari, N., Hidayatullah, R., Komarudin, N., Yolanda, Y. (2023). Liquid Waste Treatment for Sustainable Tapioca Industry: A Comparison between Biogas and Liquid Sugar. ASEAN *Journal on Science and Technology for Development, 40*(1), 9–19. https://doi.org/10.61931/2224-9028.1001
- Sulistyowati, L., Syarif, M., Elvira, M., Putrianti, N., Andareswari, N., Krisnawati, E., Komarudin, N. (2024). From Waste to Wealth: Entrepreneurial

- Ventures in Chitosan Extraction for Environmental Sustainability. *APTISI Transactions on Technopreneurship (ATT)*, 6(3), 443–457. https://doi.org/10.34306/att.v6i3.480
- 56. Triola, M. (2018). *Statistics*. (10<sup>a</sup> ed.). Addison-Wesley (in Spanish). https://www.uv.mx/rmipe/files/2015/09/estadistica.pdf
- 57. Tursi, A., Maiorano, P., Sion, L., D'Onghia, G. (2015). Fishery resources: between ecology and economy. *Rendiconti Lincei*, 26(1), 73–79. https://doi.org/10.1007/s12210-014-0372-3
- 58. Wagh, M., Aher, Y., Mandalik, A. (2022). Potential of *Moringa Oleifera* Seed as a natural adsorbent for wastewater treatment. *Trends in Sciences*, *19*(2). https://doi.org/10.48048/tis.2022.2019
- 59. Winfield, J., Greenman, J., Dennis, J., Ieropoulos, I. (2016). Analysis of microbial fuel cell operation in acidic conditions using the flocculating agent ferric chloride. *Journal of Chemical Technology & Biotechnology, 91*(1), 138–143. https://doi.org/10.1002/jctb.4552
- 60. Worku, G., Abate, S. (2025). Efficiency comparison of natural coagulants (Cactus pads and Moringa seeds) for treating textile wastewater (in the case of Kombolcha textile industry). *Heliyon*, *11*(4), 1-19. https://doi.org/10.1016/j.heliyon.2025.e42379
- 61. Yang, R., Li, H., Huang, M., Yang, H., Li, A. (2016). A review on chitosan-based flocculants and their applications in water treatment. *Water Research*, *95*(1), 59–89. https://doi.org/10.1016/j. watres.2016.02.068